



Hydrogen Storage in Hydrides for Safe Energy Systems

A Consortium of EC FP5, programme 1998-2002, funded for the period 2002-2005

Partners are :

IFE – Norway (coordinator) – WP6

Stockholms University – Sweden – WP3

CNRS Grenoble – France – WP1, WP2

NCSR D – Greece (management)

Treibacher Industrie – Austria – WP4

MCPT – France

Statkraft – Norway

ABB – Sweden – WP5

Kockums - Sweden / **HDW** - Germany

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Three classes materials were proposed for fundamental studies and research development for applications. (WP1 to 3)

Processing and upscale of the materials and hydrides were planned operating by specialised industrial companies from pilot, then to mass production. Parallel to numerical modelisation of the mass, heat and pressure transfers, developments of metal hydride tanks was proposed. (WP4)

As fuel cells were considered for a practical end-use, a large tank development was made, then for further connection to a multimode safe energy system. (WP5)



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A **1st class metal hydride of BCC type**, aims to achieve better than 2 w%, reversible properties at e.g. 80°C in a first step, then even closer to RT. Syntheses were oriented to optimise a multinary aspects of the alloys, in terms of formula and processes (milling and melting), thus to achieve fast kinetics of absorp./desorp. A pilot scale production was also done and critically analysed.

A **2nd class of material considered is Mg-activated hydride**, for which the performance of more than 6 w% were fully realised in both the laboratory and in safe industrial pilot process for mass production.

A **3rd class of materials comprises different light materials** e.g. Li and Na alanates and more complex types multinary metals hydrides, thus potentially able to develop a max H-uptake ranging from 5 to 10 w%. They were expected to achieve high reversible performances specifically down to 140°-150°C.



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The BCC type hydride was designed for static systems and the latter two classes aim to be used for fuelling mobile applications.

Upscale pilot production of these materials was operated on the basis of optimised properties resulting from basis studies.

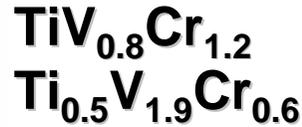
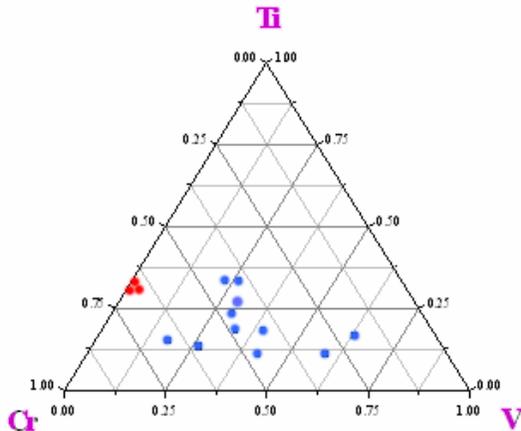
Numerical computation were made using 2D numerical codes to **simulate tank working conditions**. **Development of prototype tanks** (lab and factory scale) were realised in order to qualify the active materials, thus monitoring work parameters (pressure, cold and heat transfers, thermal gradient, time...).

A **large scale tank** was constructed, charged with hydrides then **being connected to a fuel cell** as a part of a complex energy management system for a 4-floor building in Stockholm.

The major results gained during the first 2 years of the **HYSTORY** workplan are discussed here after.

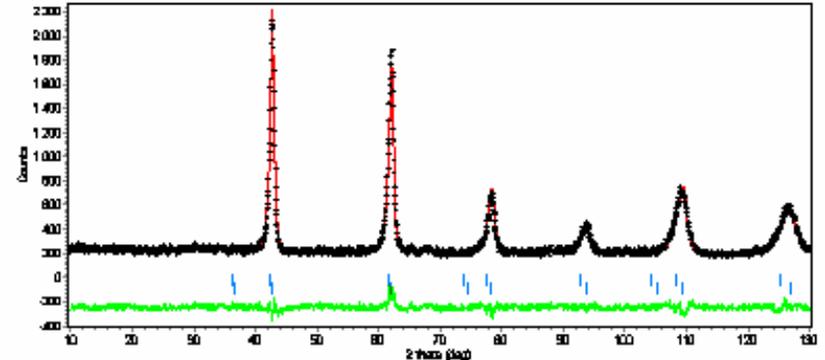
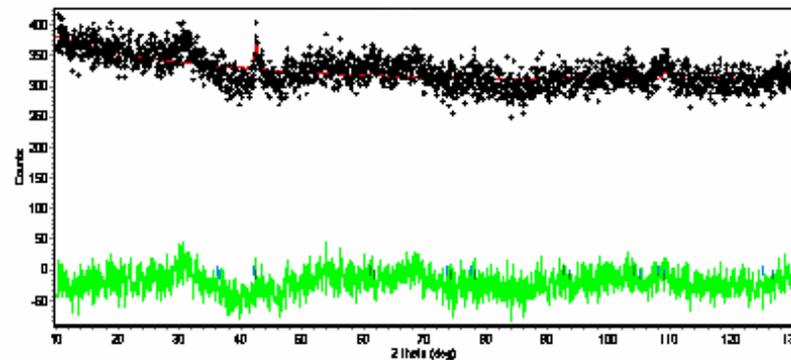
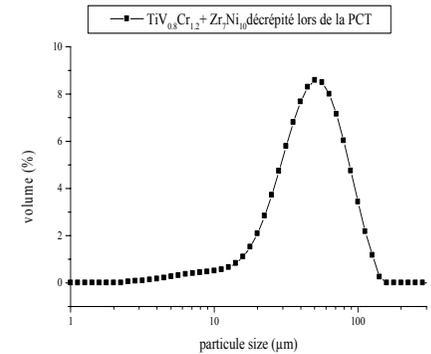
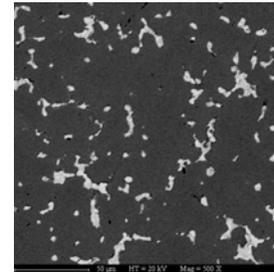
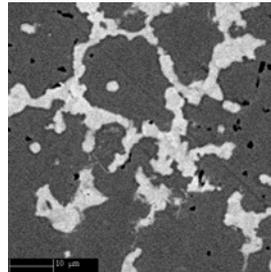
HYSTORY

Class A metal hydrides from BCC type alloys



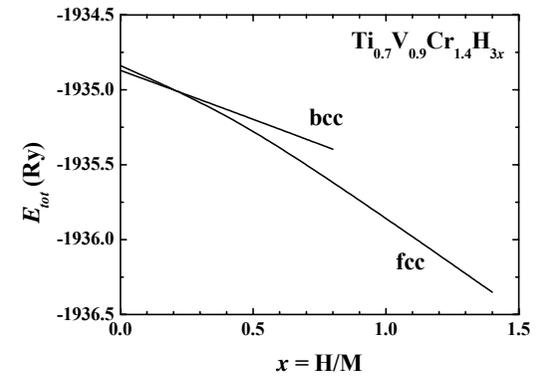
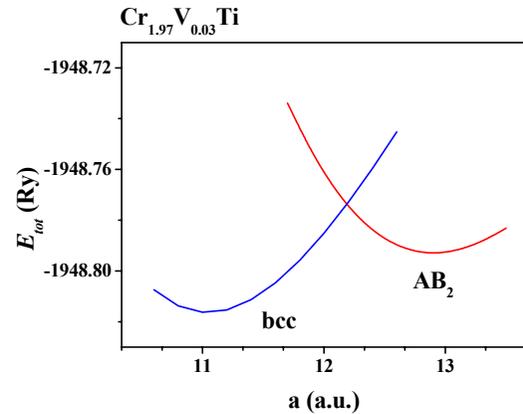
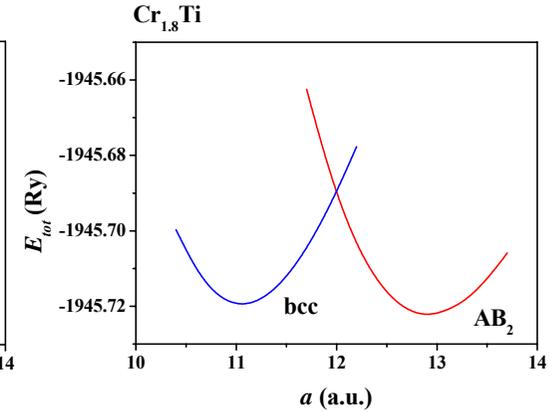
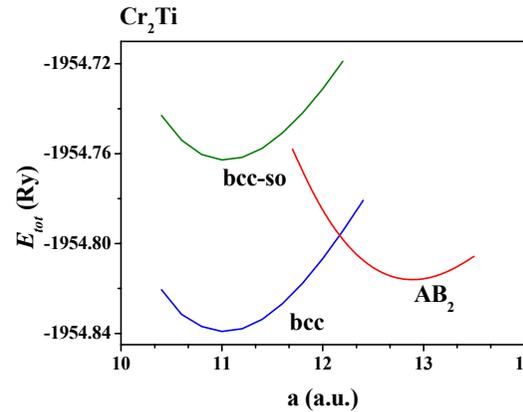
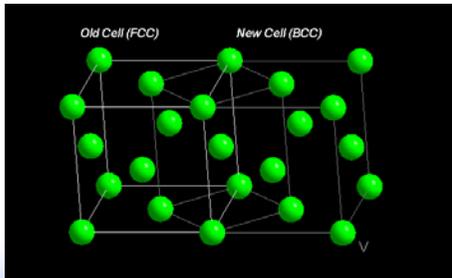
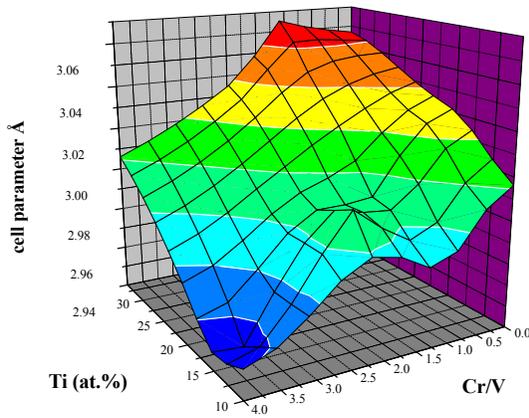
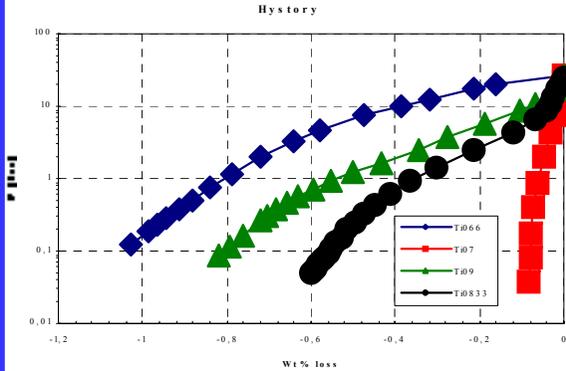
$X_{max} \sim 3.1w\% \dots$ up to...

$X_{max} \sim 3.6w\%$

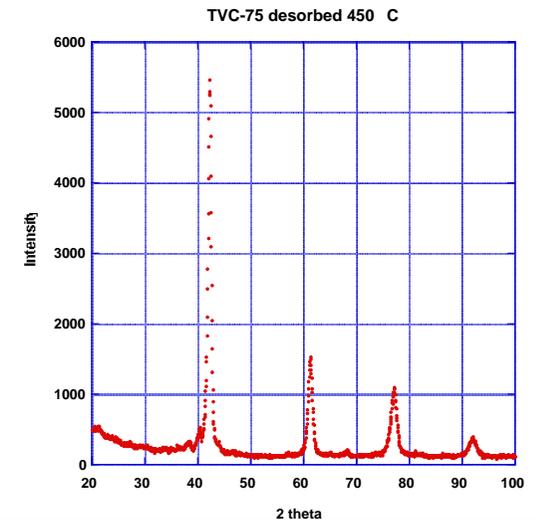
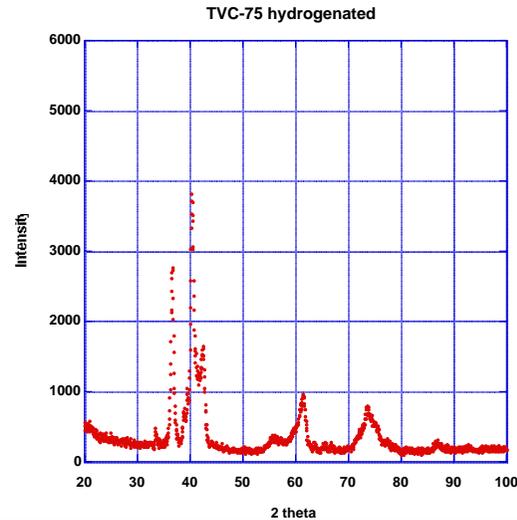
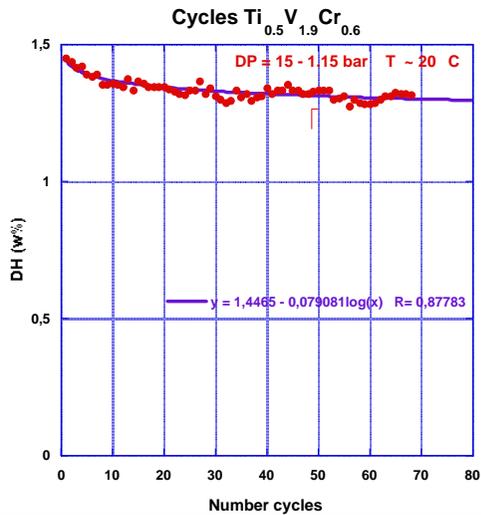
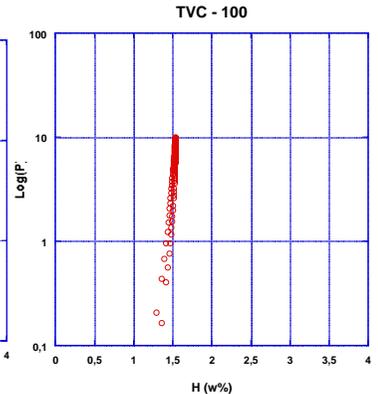
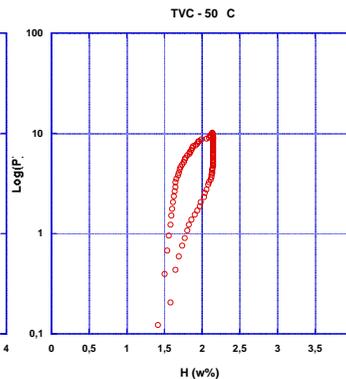
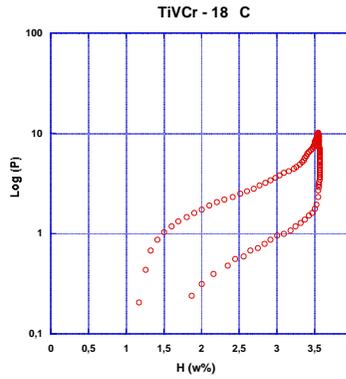
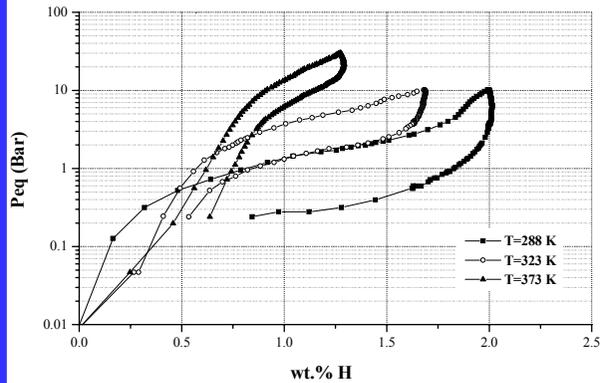


HYSTORY

Class A metal hydrides from BCC type alloys

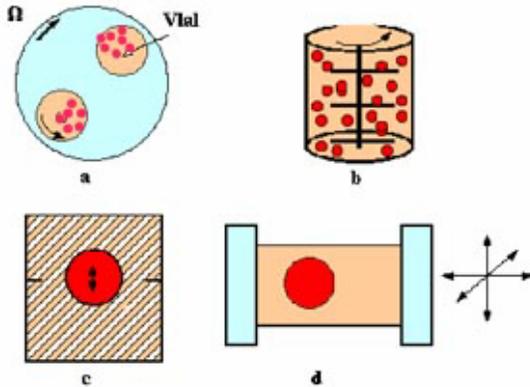


Class A metal hydrides from BCC type alloys



HYSTORY

Class B metal hydrides as activated $Mg(X)H_2$



Co-milling of MgH_2 powders with activating early d-metal or d-metal compoundse.g. oxides....

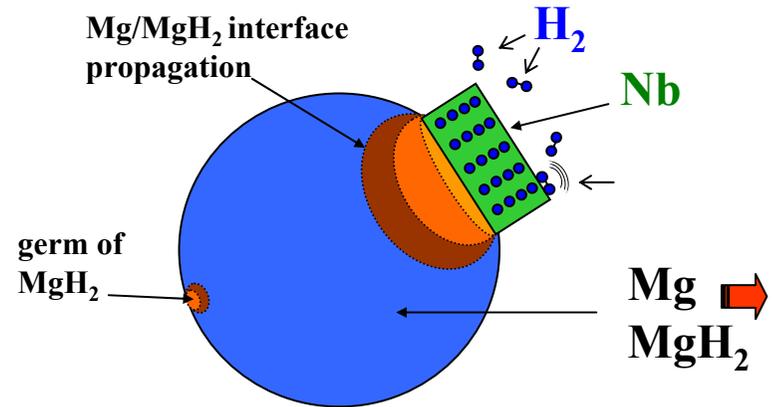
T = Ti, V, Nb.. are active (larger is the valence state better the d-metal is active).

WE CHOOSE PURE METALS SINCE OXIDES (V_2O_5 , Cr_2O_3 ..) ARE KNOWN HIGH CARCIGEN..!

Several aspects in ball-milling :
creation of high density of defects
creation of nanoscale M/ MgH_2 interfaces

Important :
energy of co-milling
time of milling
amount of activant

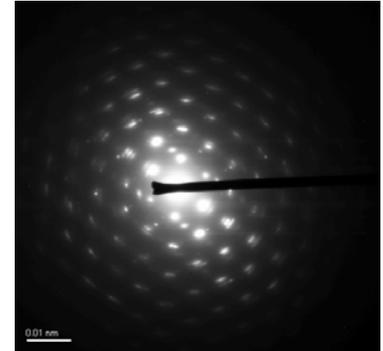
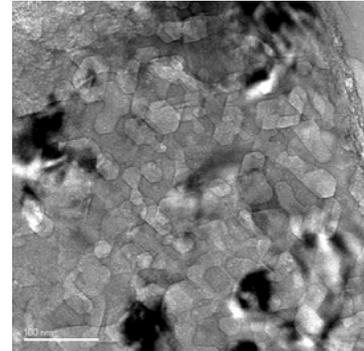
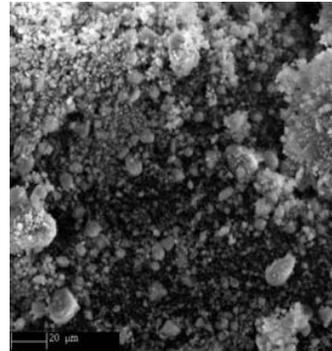
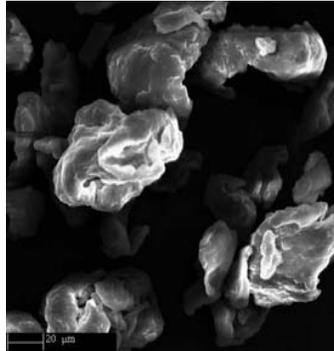
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Scheme for a Nb nano-particle interfacing a micrometric Mg grain

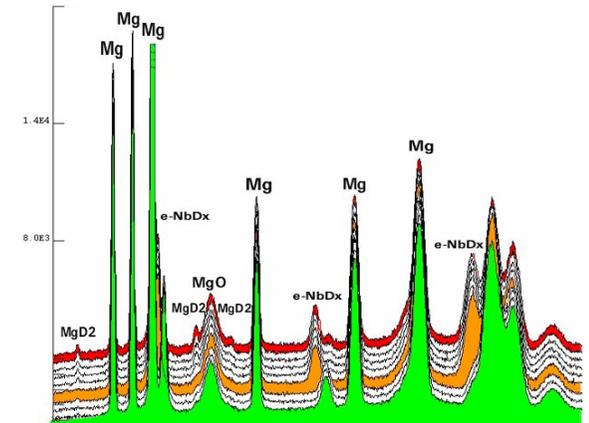
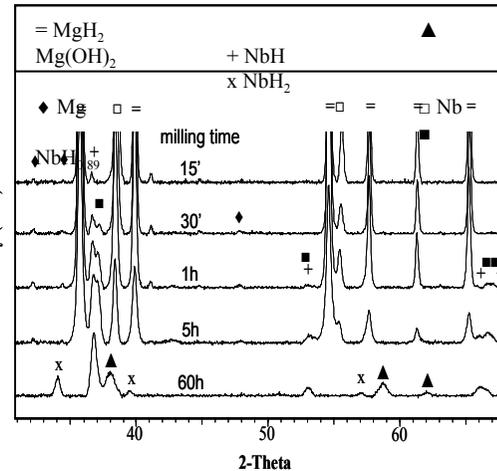
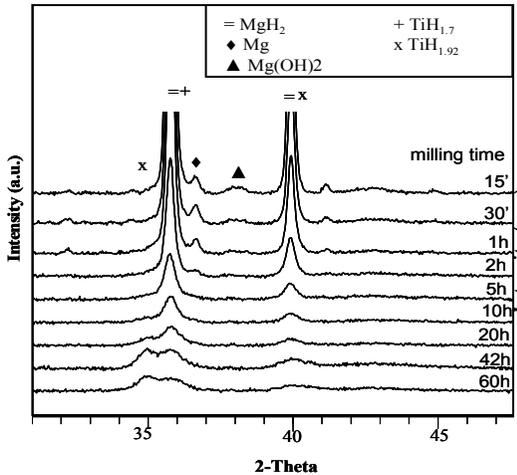
HYSTORY

Class B metal hydrides as activated $Mg(X)H_2$



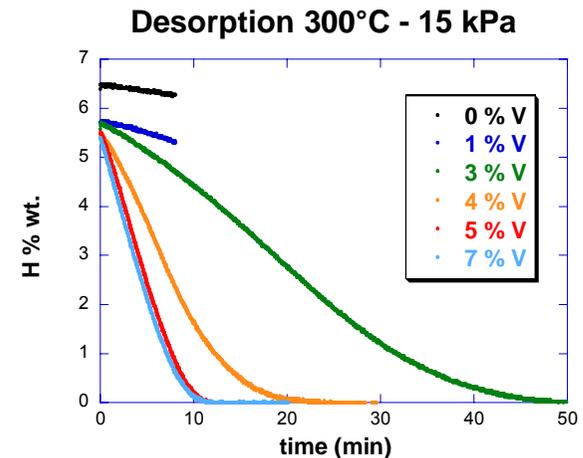
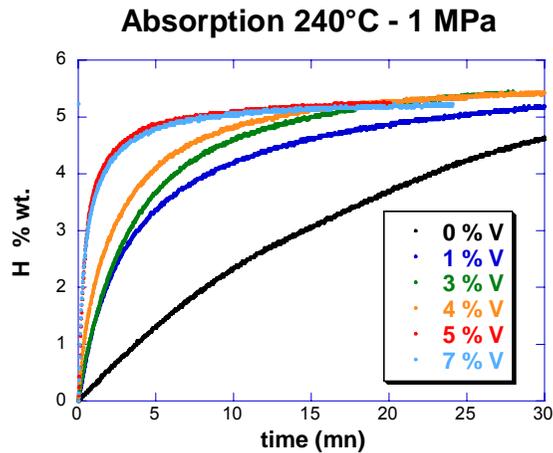
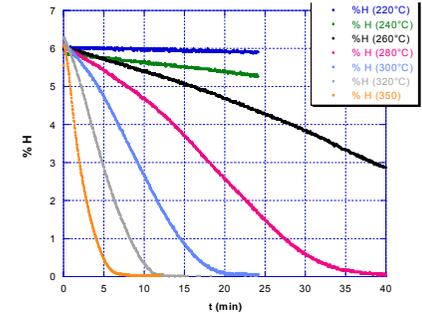
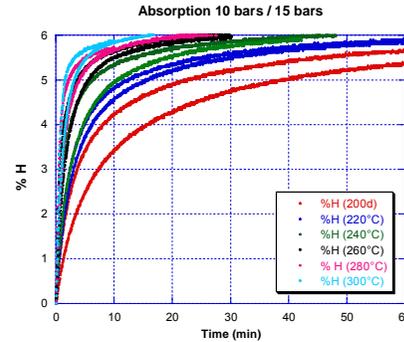
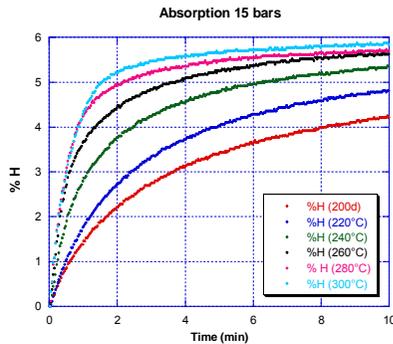
a - SEM picture of as received MgH_2 , the mean grain size is up to $40 \mu m$, b - SEM picture of a 100 hour ball milled MgH_2 the mean size distribution range from 0.2 to $10 \mu m$.

c - HREM picture of a 60 hour ball milled MgH_2 , which defects and nano crystalline state is transformed to well shaped and homogeneous size crystals after evacuation under beam; mean grain size $\sim 20 nm$. d - Electr. diffraction picture of in-situ well recrystallised Mg from MgH_2 precursor.



X-ray and neutron diffraction experiments revealing the formation of MH_x phase during the ball-milling (activation), and at hydrogen absorption/desorption process (active interface)

Class B metal hydrides as activated $Mg(X)H_2$



Optimised activated materials : 1 - $Mg(V)H_2$ leads to react promptly at 50°C for absorption, 2 - desorption can be promoted significantly fast at 220°C

Class B metal hydrides as activated $Mg(X)H_2$

Empirical kinetics laws : $x (t, T, P)$

$x =$ fraction of Mg transformed to MgH_2 at a time t

Absorption : Jander law

hydrogen diffusion through the MgH_2 layer

$$(1 - (1-x)^{1/3})^2 = k \cdot t$$

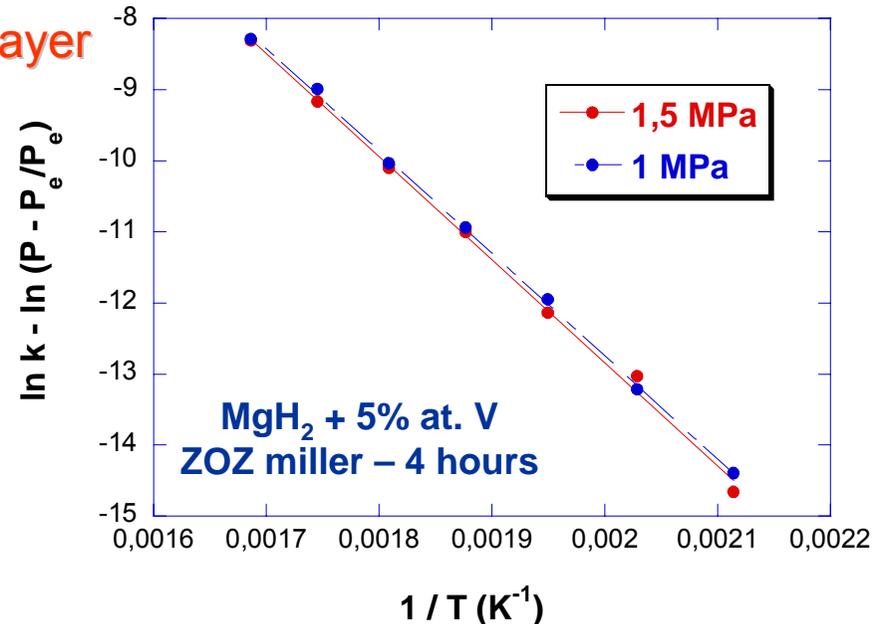
$$k = k_0 \cdot (P - P_e) / P_e \cdot \exp(-E_a / RT)$$

$$\left\{ \begin{array}{l} E_a = 120 \text{ kJ / mol } H_2 \\ k_0 = 9.9 \cdot 10^6 \text{ s}^{-1} \end{array} \right.$$

Desorption :

$$(1-x)^{1/3} = k \cdot t$$

$$k = k_0 \cdot \exp(-E_a / RT)$$

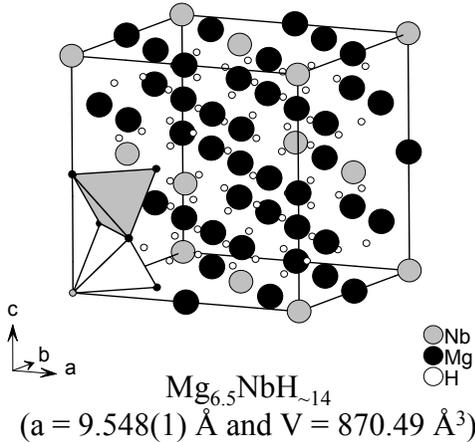


$$\left\{ \begin{array}{l} E_a = 95 \text{ kJ / mol } H_2 \\ k_0 = 0.25 \cdot 10^6 \text{ s}^{-1} \end{array} \right.$$

Class B Mg-based metal hydrides

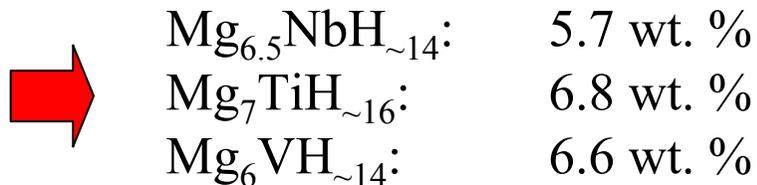
FCC structure (metal structure: Ca₇Ge type structure)

Crystallographic parameters for Mg_{6.5}NbH_{~14} in space group Fm-3m (No. 225) and Z = 4



Atom	Site	x	y	z	B _{iso}	Occupancy
Nb	4a	0	0	0	1.2(1)	1.00
Mg1	4b	1/2	1/2	1/2	0.5(1)	0.52(2)
Mg2	24d	0	1/4	1/4	0.5(1)	1.00
H1	32f	0.127(4)	0.127(4)	0.127(4)	3.0	1.00
H2	32f	0.360(3)	0.360(3)	0.360(0)	3.0	1.00

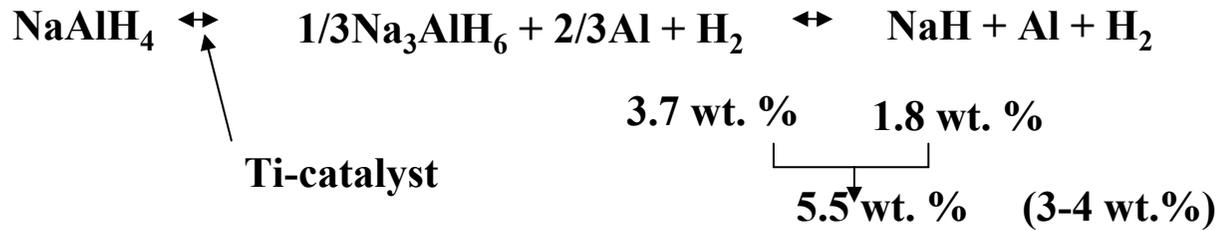
The new metal hydrides with FCC structure have high hydrogen contents



Class C : Alanates as light metal hydrides

	Dehydrogenation temperature (°C)	Hydrogenation		Hydrogen content (wt.%)
		Temperature (°C)	Pressure (bar)	
LiAlH_4	-	-	-	10.5
NaAlH_4	< 160	120-130	< 120	7.4
KAlH_4	300	> 300	100	5.7

NaAlH_4 : High hydrogen contents & reversible



LiAlH_4 : low stability and poor reversibility

NaAlH_4 : looks the best candidate

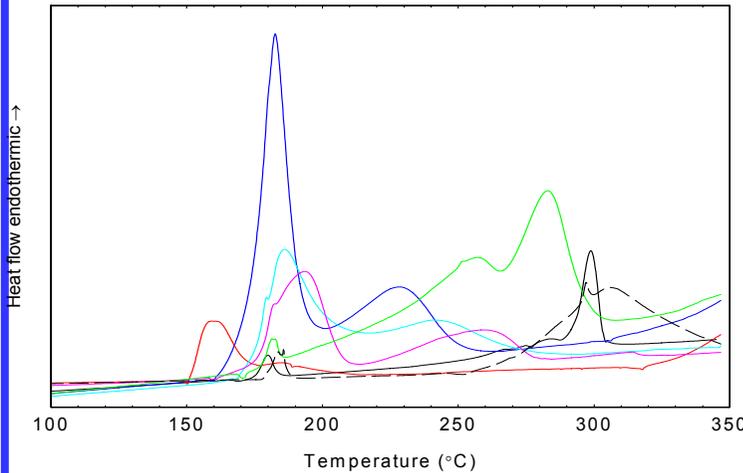
KAlH_4 : high temperature dehydrogenation for low H content

Main problems : low kinetics! needs catalytic activation!

-> What catalysts? Mixed alkali-metal systems : structure and kinetics

Class C : Alanates as light metal hydrides

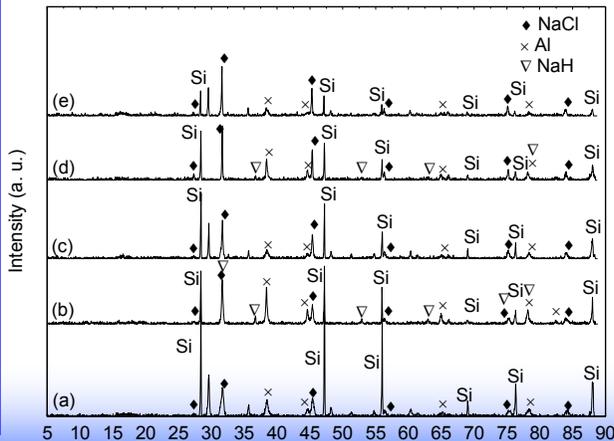
Dehydrogenation kinetics for Ti-catalyst doped/undoped NaAlH₄



*heating rate: 10 °C/min in Ar gas flow

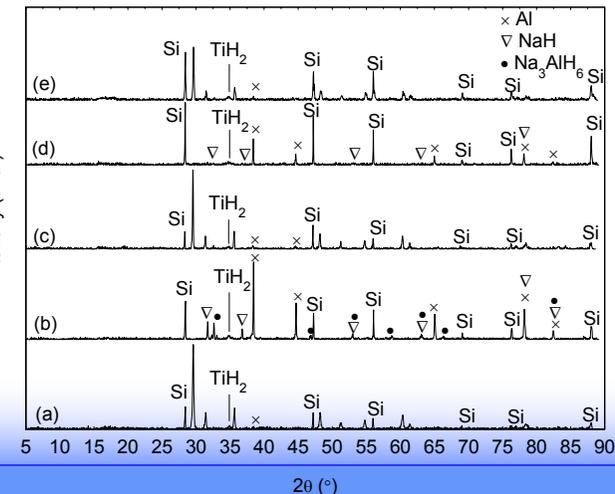
Catalyst	Onset temperature (°C)
Pure NaAlH ₄ (⋯)	177.31
Ball milled NaAlH ₄ (—)	175.66
Ti (—)	178.14
★ Nanosized activated Ti (—)	159.31
TiH ₂ (—)	176.66
TiC/TiN (—)	166.52
★ TiCl ₃ -1/3AlCl ₃ (—)	151.24

Cycling



Dehydrogenation: 160°C
and 1 bar for 2 h;
Hydrogenation: 125°C and
< 110 bar in H₂ for 24 h.

Ball milled (a), after 1st
dehydrogenated (b), 1st cycled
(c) 10th dehydrogenated (d) and
11th cycled (e) sample



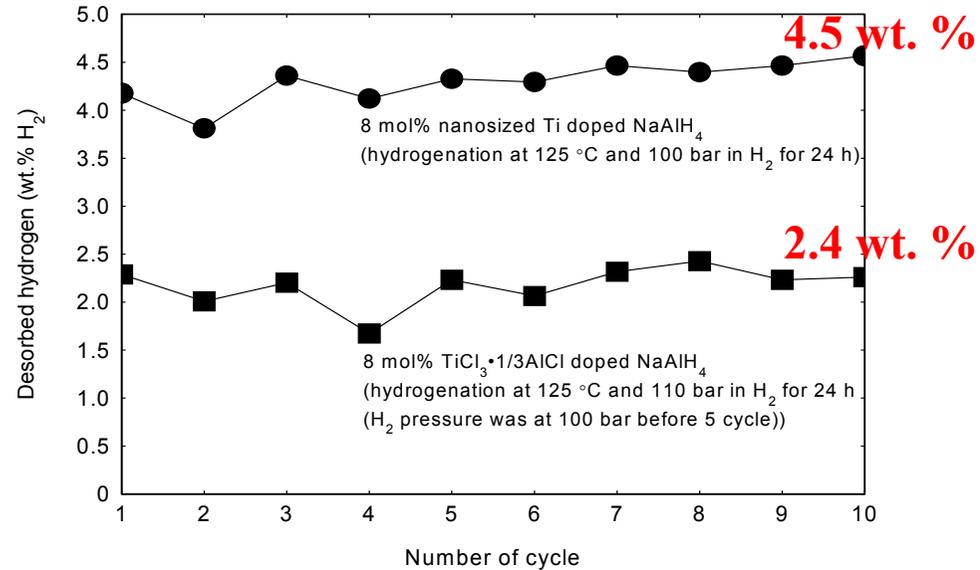
Class C : Alanates as light metal hydrides

Amount of desorbed hydrogen

Ball milled ordinary Ti doped NaAlH_4

≤ 3.75 wt. %

(P. Wang and C. M. Jensen, *J. Phys. Chem. B* 2004, 108, 15827.)



Conclusions

NaAlH_4 with dispersed Ti (< 100 nm)

Better reversibility and high hydrogen content (4.5 wt. %)

Desorption (160 °C/1 bar for 2h)/Absorption (125 °C/100 bar for 24h)

Large amounts of the sample can be made by ball milling

KAID_4 and studies of Al phases and crystal quality related to the reactions

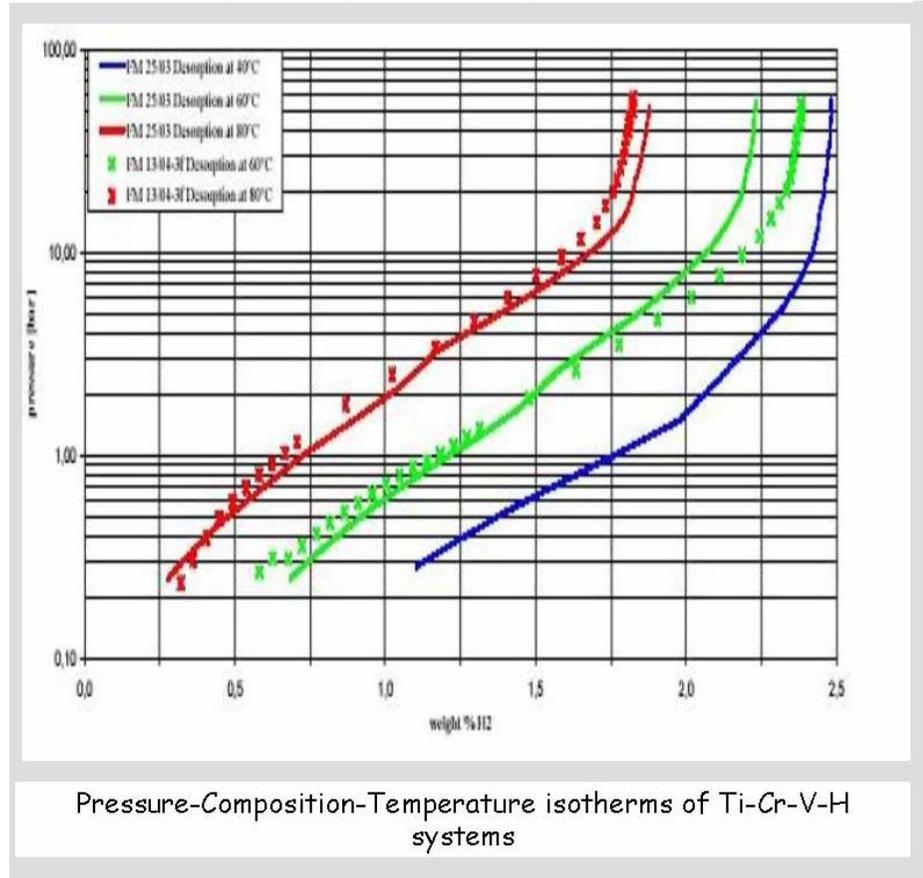
The life cycling operation was performed up to 10 cycles

Upscale class A materials

Presently, batches of ~ 20 kg have been produced at Treibacher Industry plant. However the first alloys as studied in the Hystory project were not formulated specially for fuel-cell operation. New batches are under synthesis, developed from the most recently prepared formulas (temperature range : 20-60°C)



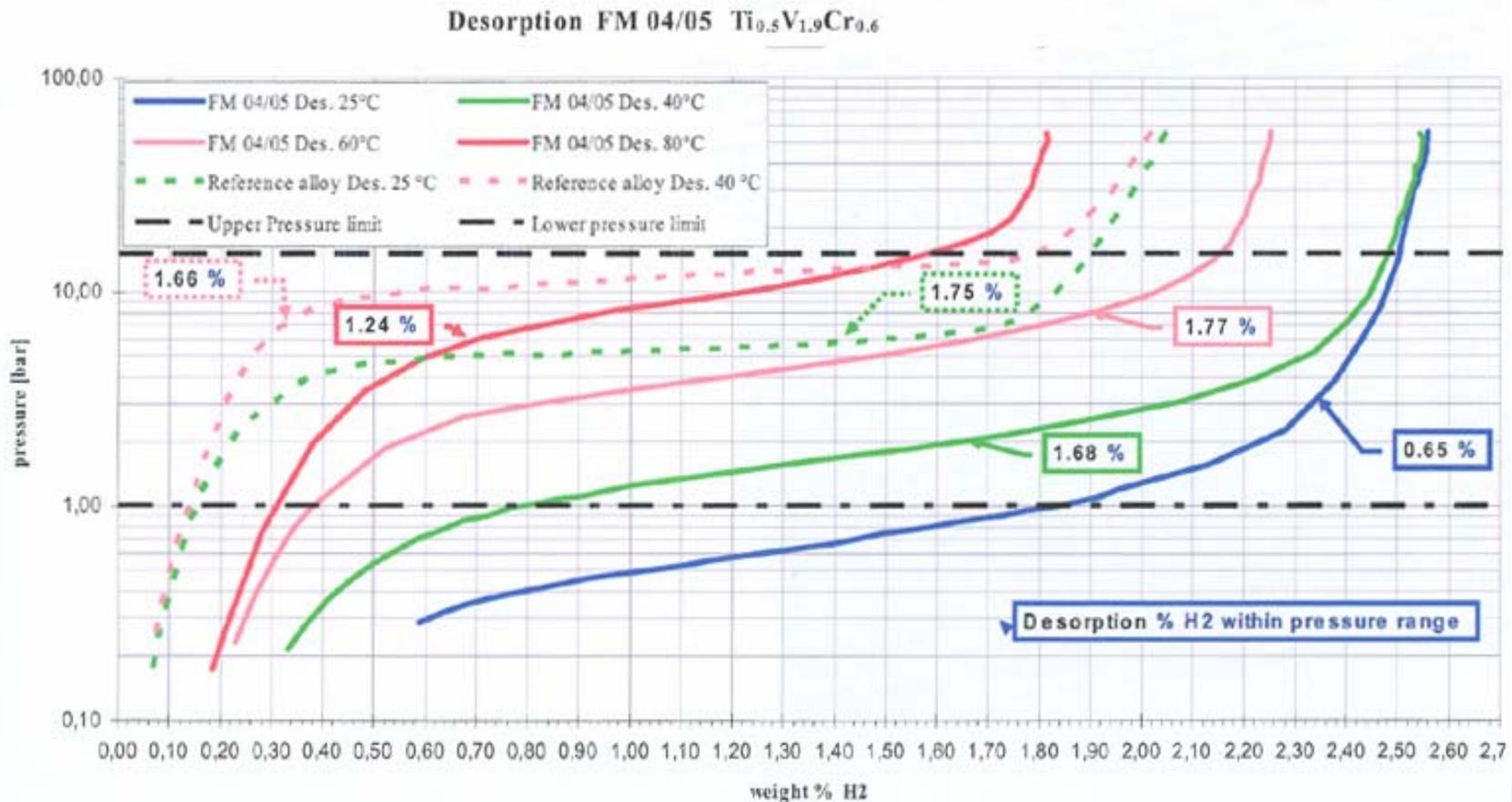
Small scale tank designed for testing the new materials within the HYSTORY project.



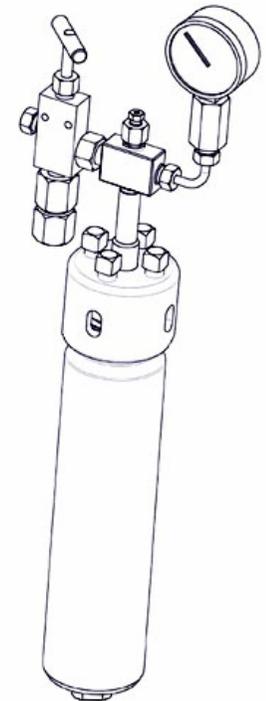
PCT measurements on a Ti-rich BCC alloy as prepared at Treibacher Industrie

Upscale class A materials

A new BCC type hydride behave better than the « conventionnal » AB_2H_x as delivered for the large tank designed for fuel cell application.



Upscale class B materials



Rotating furnace and autoclave with its ancillary equipments installed at MCPT to prepare the MgH_2 precursor from Mg powder

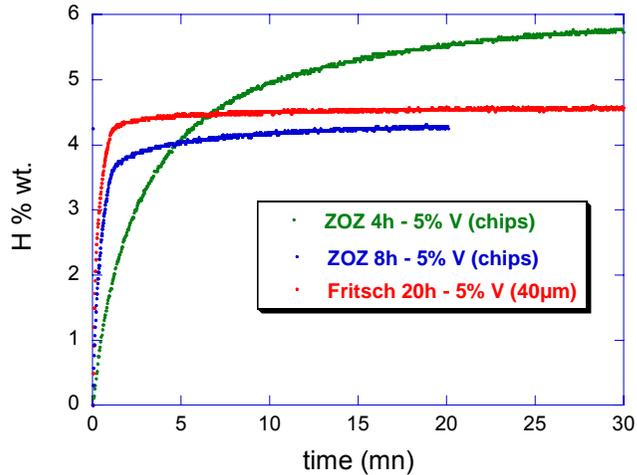
Upscale class B materials



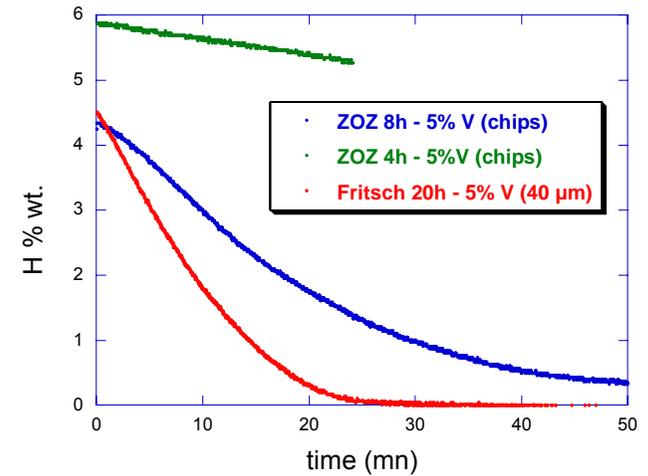
Large scale energetic ball miller (ZOZ) used to prepare kg batches of M-activated MgH_2

Upscale class B materials Comparisons Institute/Industry

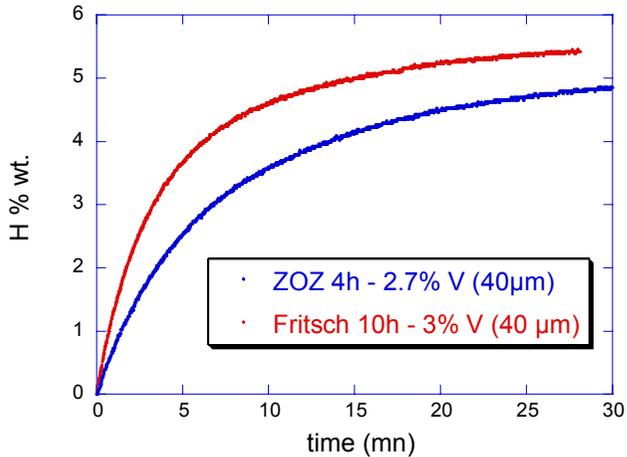
Absorption 240°C - 1 MPa



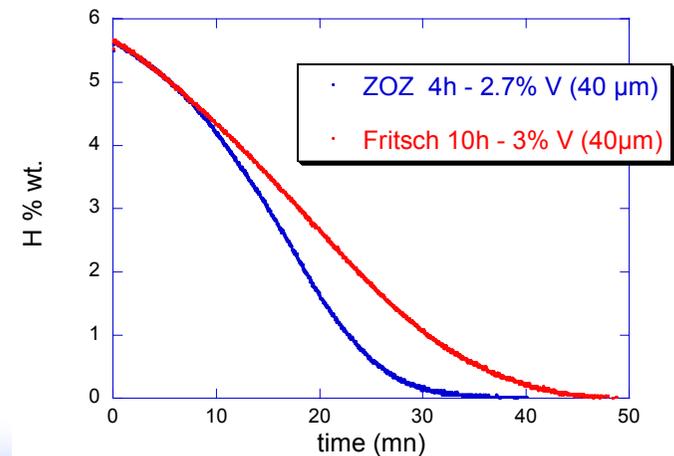
Desorption 240°C - 15 kPa



Absorption 240°C - 1 MPa



Desorption 300°C - 15 kPa





Simulation of tank in working conditions

Need for optimal/safe heat management strategies and novel cost effective design options (develop new 2-D models and utilize recent advances in Dynamic Optimisation)

Bed filled with a metal hydride alloy surrounded by a cooling jacket:

Solid and gas temperatures equal

Axial and radial dispersion included

Axial and radial velocity calculated through Darcy's law or the Blake-Kozeny equation

Ideal gas law in the gas phase

Mass balance of hydrogen in the gas phase (bulk of the reactor)

Pressure Drop Equations

Energy Balance

Mass balance of hydrogen in metal phase

Definition of Equilibrium Pressure (Jemni and Nasrallah, 1995)

Other auxiliary expressions

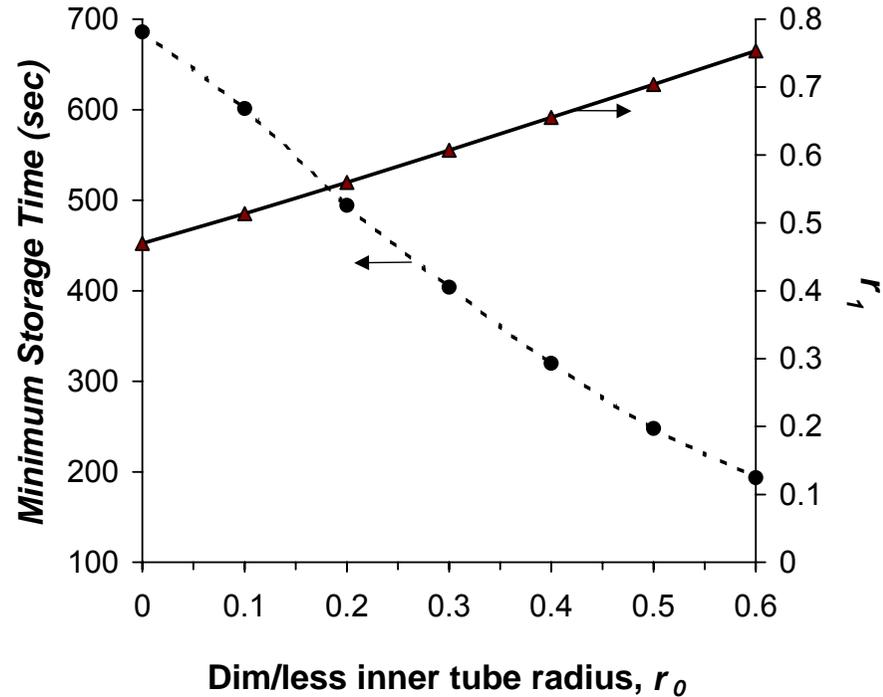
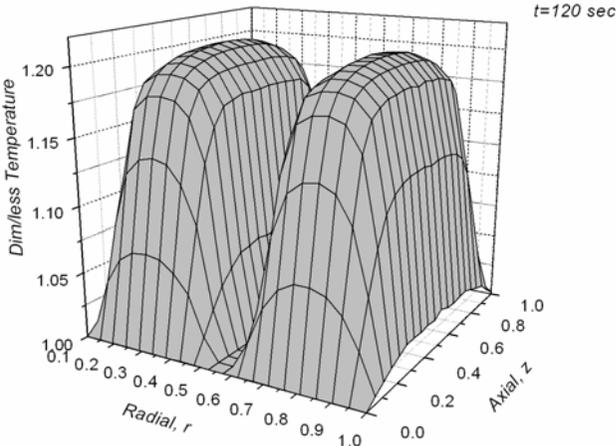
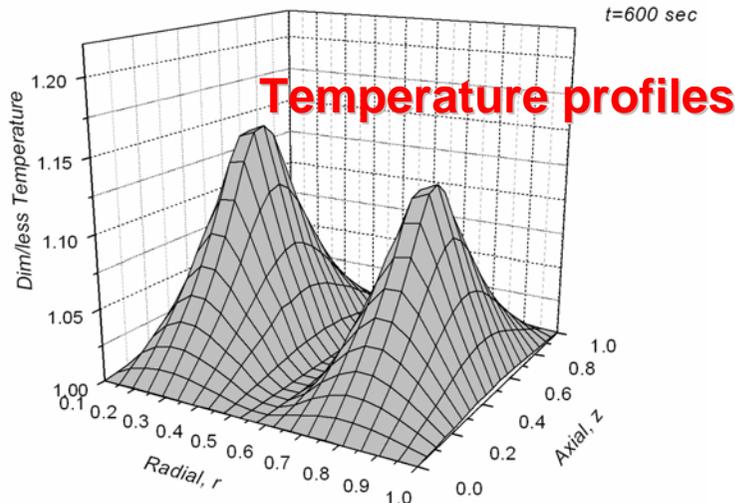
Boundary conditions

Initial Conditions

Simulation of tank in working conditions

Simulation results: 2-D H₂ storage
with annular ring heat exchanger

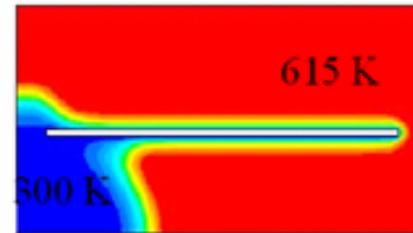
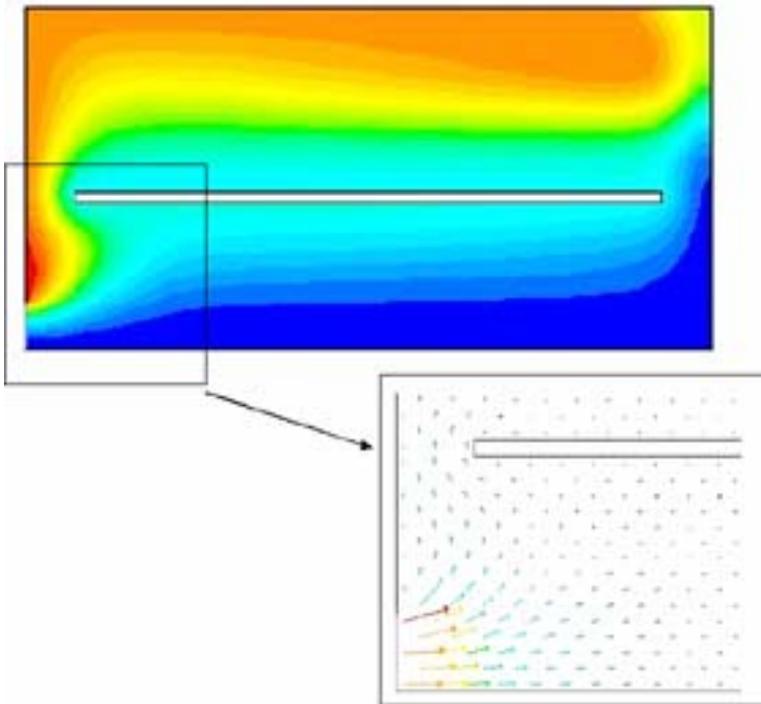
Optimal Design of the annular
ring heat exchanger



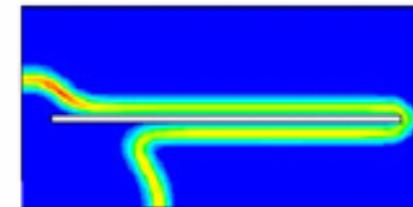
HYSTORY

Simulation of tank in working conditions

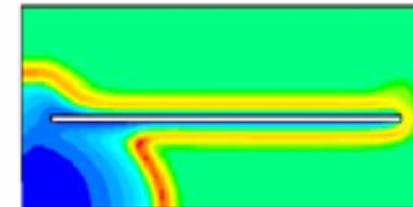
velocity streamlines



Contours of temperature

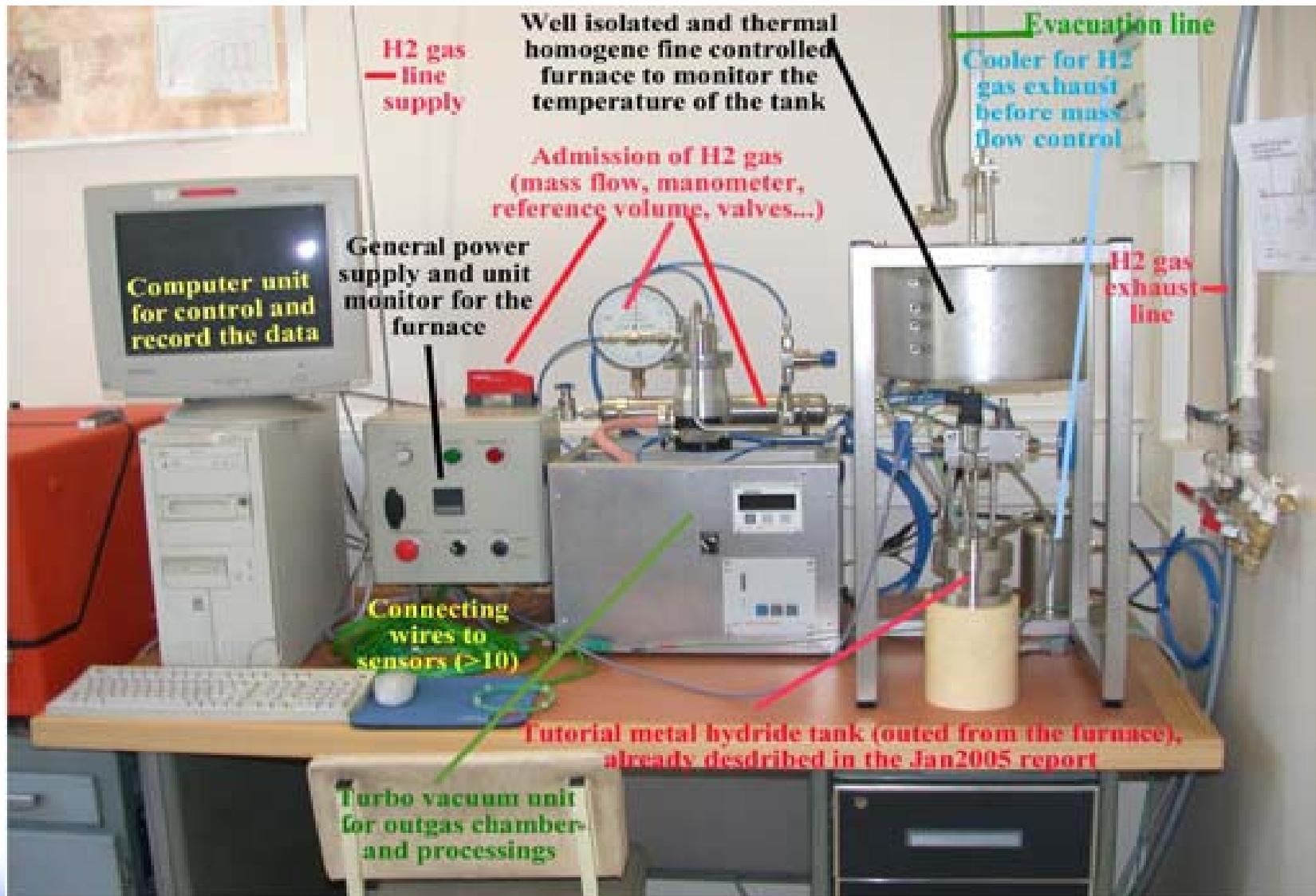


Contours of reaction rate



Contours of hydriding fraction

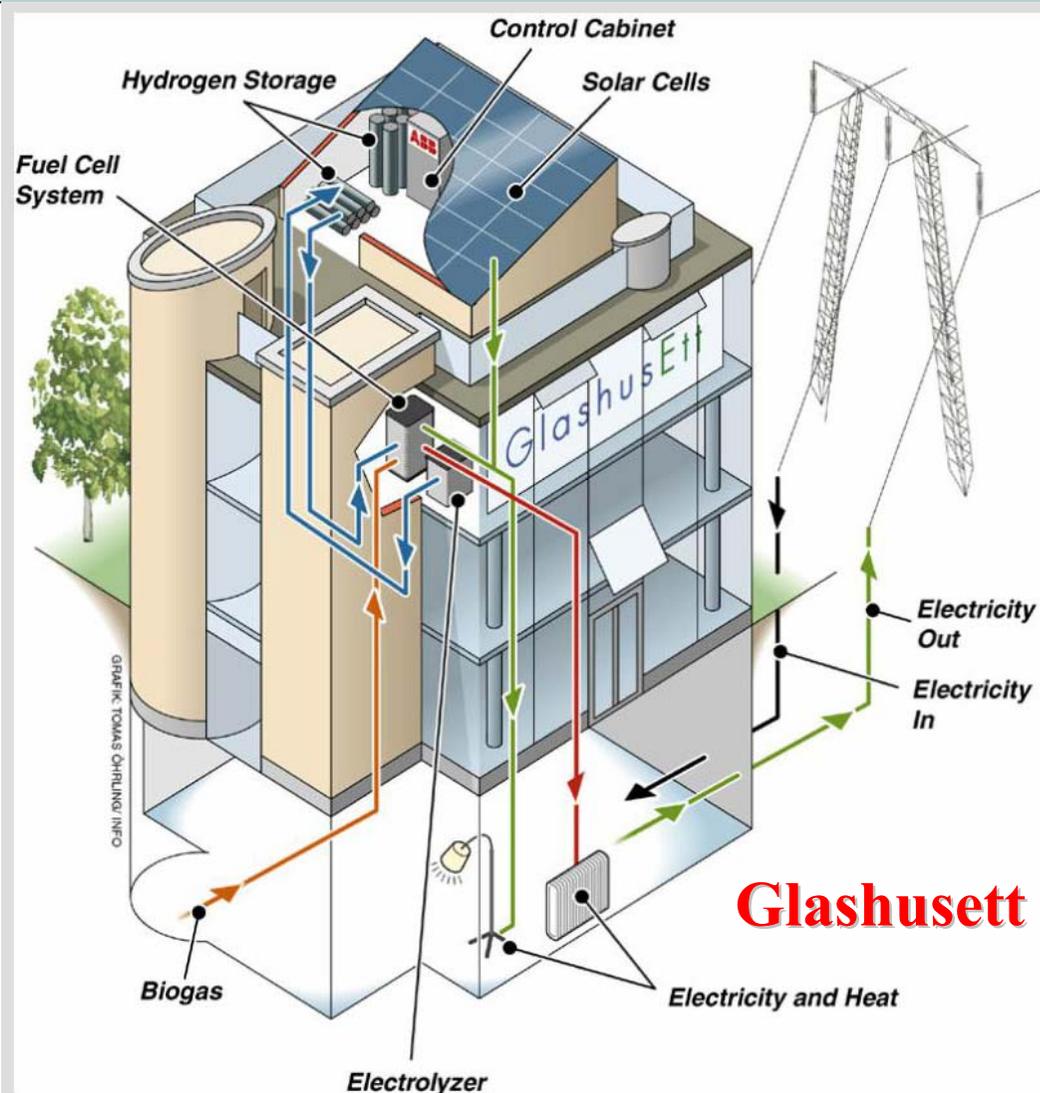
Development of a tutorial tank



Development of a full scale tank



HYSTORY



Glashusett - Stockholm

GlashusEtt in Hammarby Sjöstad, Stockholm, Sweden. Schematic drawing showing the components and the energy flow in the alternative energy system in GlashusEtt.

Glashusett - Stockholm

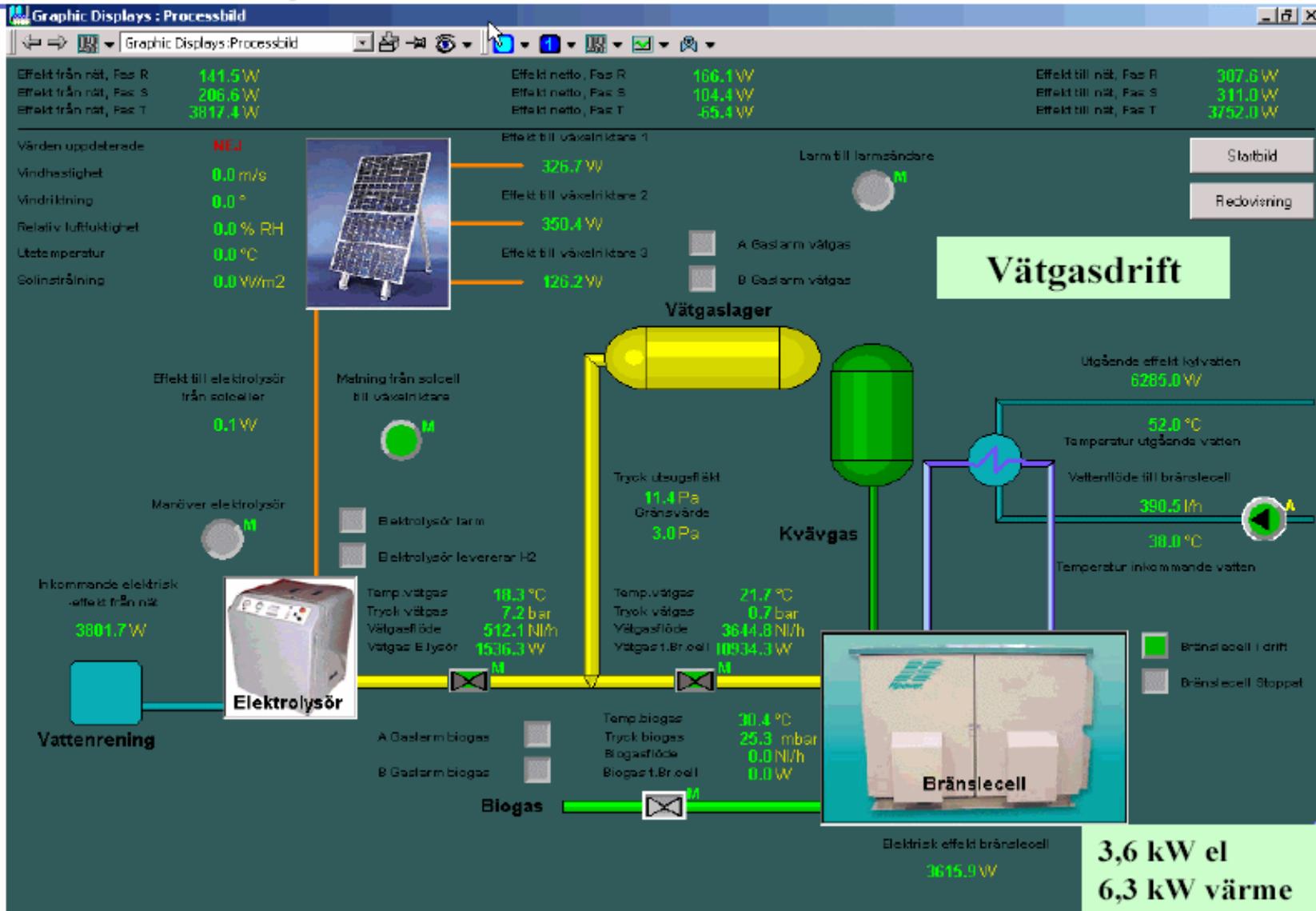


Current hydrogen storage unit in GlashusEtt: Conventional H_2 storage consisting of 22 bottles, each with a water volume of 50 litres, giving a total volume of 1100 litres. At 14 barg this storage contains 15 Nm^3 of H_2 .



Large scale metal hydride tank designed to store 15 Nm^3 of H_2 . The outer volume of the tank is approximately 90 litres. This tank is shortly to be installed in GlashusEtt.

Kontrollsystem – Processbild





HYSTORY



To Achieve

Optimised formula in the Ti-V-Cr systems with a large FCC-hydride ~ RT
Upscaling the BCC type of alloys and hydrides
Development of a prototype large tank

Nature and structure of the M/MgH₂ active interface (Ti-Mg hydride?)
Better and new catalysts for Mg-activation
Upscaling the Mg(M)H₂ production
Simulation and experience in tank management (matter and heat exchange...)
Development of large tank (~ 5 kg MgH₂)

Mixed alkali-alanates
About the Ti catalytic effect in alanates (Al metastable alloy)
Experience in tutorial tank



EC FP 5
Programme
1998-2002

HYSTORY



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Thank you
for your attention



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